

# Cooling Tower Efficiency Calculations

Cooling Tower Efficiency Calculation is described in this article. Cooling Tower plays a major role in Chemical Process Industry. They reject process heat from the cooling water to atmosphere and keep the water cool. The performance of the cooling tower depends on various parameters like Range & Approach. We shall see those terminologies in Detail.

## Cooling Tower Approach:

The difference between the Cold Water Temperature (Cooling Tower Outlet) And ambient Wet Bulb Temperature is called as Cooling Tower Approach.

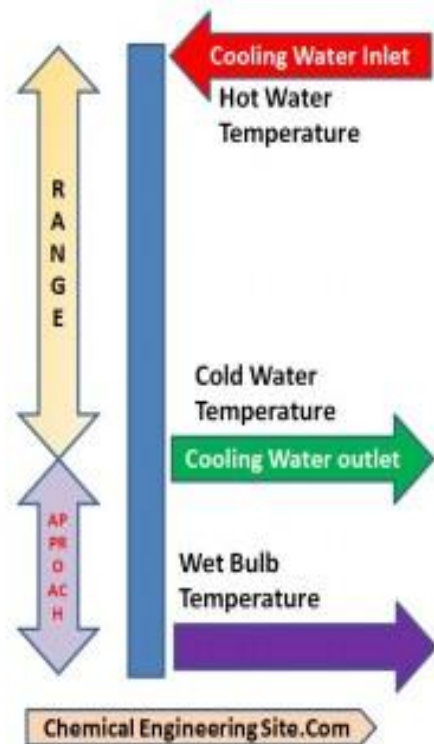
$$\text{Approach} = \text{Cold Water Temperature} - \text{Wet Bulb Temperature}$$

Cooling Tower approach is the better indicator for the performance.

## Cooling Tower Range:

The difference between the Hot Water Temperature (Cooling Tower Inlet) Temperature and Cold water (Cooling Tower Outlet) temperature is called Cooling Tower Range.

$$\text{Range} = \text{Hot Water Temperature} - \text{Cold Water Temperature}$$



## Cooling Tower Efficiency Calculation:

The calculation of cooling tower efficiency involves the Range and approach of the cooling Tower. Cooling tower efficiency is limited by the ambient wet bulb temperature. In ideal case the cold water temperature will be equal to the wet bulb temperature. This is practically not possible to achieve. This

requires very large tower and results in huge evaporation and windage or drift loss resulting in a practically not viable solution. In practice the cooling tower efficiency will be in between 70 to 75%.

**Cooling Tower Efficiency =**

**$(\text{Hot Water Temperature} - \text{Cold water Temperature}) \times 100 /$**

**$(\text{Hot Water Temperature} - \text{Wet bulb temperature})$**

Or Simply

**$\text{Cooling Tower Efficiency} = \text{Range} / (\text{Range} + \text{Approach}) \times 100$**

In summer the ambient air wet bulb temperature raises when compared to winter thus limiting the cooling tower efficiency.

## Other Cooling Tower Calculations:

This includes determination of cycle of concentration, Evaporation loss, Drift or Windage Loss, Blow down water requirement Make up water requirement.

### Cycle of Concentration:

Cycle of concentration is a dimensionless number. It is a ratio between parameter in Cooling Water to the parameter in Makeup water. It can be calculated from any the following formulae.

$\text{COC} = \text{Silica in Cooling Water} / \text{Silica in Makeup Water}$

$\text{COC} = \text{Ca Hardness in Cooling Water} / \text{Ca Hardness in Makeup water}$

$\text{COC} = \text{Conductivity of Cooling Water} / \text{Conductivity of Makeup water}$

The cycle of concentration normally varies from 3.0 to 7.0 depending on the Process Design. It is advisable to keep the Cycle of concentration as high as possible to reduce the makeup water requirement of the cooling tower. At the same time higher cycle of concentration increases the dissolved solids concentration in circulating cooling water which results in scaling and fouling of process heat transfer equipments.

### Draw off or Blow down:

As the cooling water circulates the cooling tower part of water evaporates thereby increasing the total dissolved solids in the remaining water. To control the Cycle of Concentration blow down is given. Blow down in the is the function of Cycle of concentration. Blow down can be calculated from the formula:

$B = E / (\text{COC} - 1)$

B = Blow Down ( $\text{m}^3/\text{hr}$ )

E = Evaporation Loss ( $\text{m}^3/\text{hr}$ )

COC = Cycle of Concentration. Varies from 3.0 to 7.0 depending upon Manufactures Guidelines

### Evaporation Loss Calculation:

Evaporation Loss in cooling tower is calculated by the following empirical equation.

**$E = 0.00085 \times R \times 1.8 \times C$**

E = Evaporation Loss ( $\text{m}^3/\text{hr}$ )

R = Range

C = Circulating Cooling Water ( $\text{m}^3/\text{hr}$ )

(Reference: Perry's Chemical Engineers Hand Book )

Alternatively, The Evaporation loss can be calculated from the heat balance across the cooling tower. The amount of heat to be removed from Circulating water according to  $Q = m C_p DT$  is  $C \times C_p \times R$ . The amount of heat removed by evaporative cooling is  $Q = m \times H_v$  is  $E \times H_v$

On Equating these two, we get

$$E = C \times R \times C_p / H_v$$

E = Evaporation Loss in m<sup>3</sup>/hr

C= Cycle of Concentration

R= Range in °C

Cp = Specific Heat = 4.184 kJ / kg / °C

H<sub>v</sub> = Latent heat of vaporization = 2260 kJ / kg

### Windage or Drift Loss Calculation:

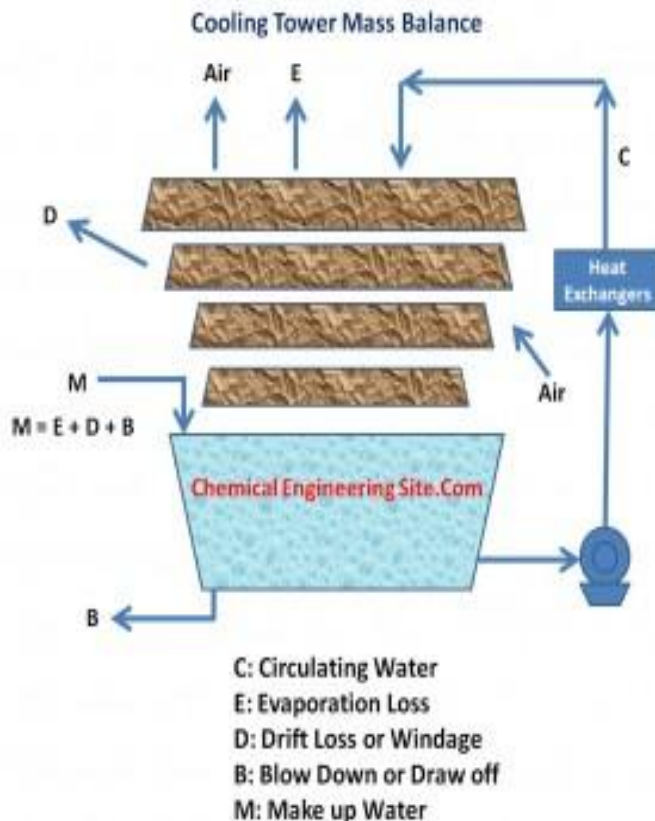
Drift loss of the cooling tower is normally provided by the cooling tower manufacturer based on the Process design. If it is not available it may be assumed as

For Natural Draft Cooling Tower  $D = 0.3 \text{ to } 1.0 * C / 100$

For Induced Draft Cooling Tower  $D = 0.1 \text{ to } 0.3 * C / 100$

For Cooling Tower with Drift Eliminator  $D = 0.01 * C / 100$

### Cooling Tower Mass Balance – Make up water:



Cooling tower mass balance gives an idea about make up water requirement. Cooling Tower Make up has to substitute the water losses resulting from Evaporation, Windage and Blow down.

$$M = E + D + B$$

M = Make up water Requirement in m<sup>3</sup>/hr

B = Blow Down in m<sup>3</sup>/hr

E = Evaporation Loss in m<sup>3</sup>/hr

D = Drift Loss in m<sup>3</sup>/hr

Source: <http://www.chemicalengineeringsite.com/cooling-tower-efficiency-calculations/76>